

# Quality Control of City Gas at Regasification Terminal

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Field Operation and Planning Sect.





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# 1.1.Self-introduction

## Shuji YAMAMOTO

<at 3 LNG Regasification Terminals for 8 years >

- 2003-2004(S) Maintenance of Instruments
- 2005-2007(S) Renewal of Control system (DCS, F&G)
- 2008(O) Construction of Regasification Plant
- 2009~2010(N) Operation & Planning

(S) : Sodegaura LNG terminal

(O) : Ohgishima LNG terminal

(N) : Negishi LNG terminal



## 1.2. Brief introduction of Tokyo Gas

### <Business areas>

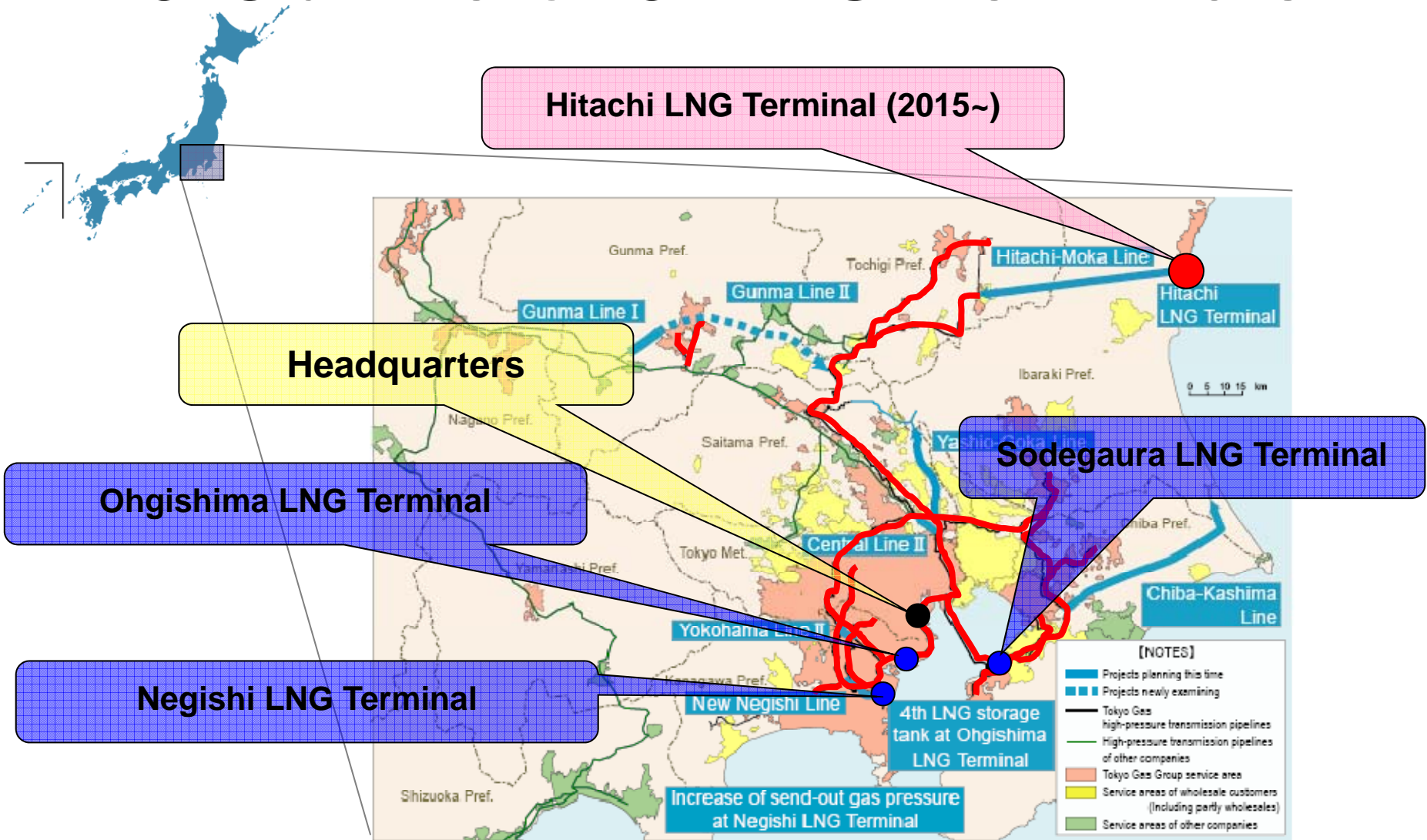
- (1) Regasification, supply and sales of city gas
- (2) Supply and sales of gas appliances
- (3) Energy services
- (4) Supply of electricity

## 1.2. Brief introduction of Tokyo Gas

### <Profile>

- Established in 1885 (**LNG, from 1969**)
- Capitalization 142 billion yen (1.2 billions Euro)
- Number of employees 15,539
- Net sales 1,416 billions yen (12 billions Euro)
- Gas sales volume 14 billions m<sup>3</sup>
- Total length of gas pipeline 57,839 km
- Number of gas customers 10,637 thousands

# 1.3. Outline of 3 LNG Terminals



# 1.3. Outline of 3 LNG Terminals

- Negishi 1<sup>st</sup> LNG receiving terminal in Japan in 1969
- Ohgishima the latest terminal in 3 terminals since 1998.
- Sodegaura one of the largest terminal in the world since 1973

**Negishi**



**Ohgishima**



**Sodegaura**







## 1.3. Outline of 3 LNG Terminals

	Negishi	Ohgishima	Sodegaura
Number of jetties	1	1	3
Number of tanks	13	3	20
Capacity of tank [MI]	1155	600	1610
Number of Vaporizers	14	10	33
Capacity of vaporizers [t/h]	1315	970	3180
Number of Employees	135	69	158
Number of Vessels ann	78	41	206
Total LNG ann [kt]	3275	2446	4577



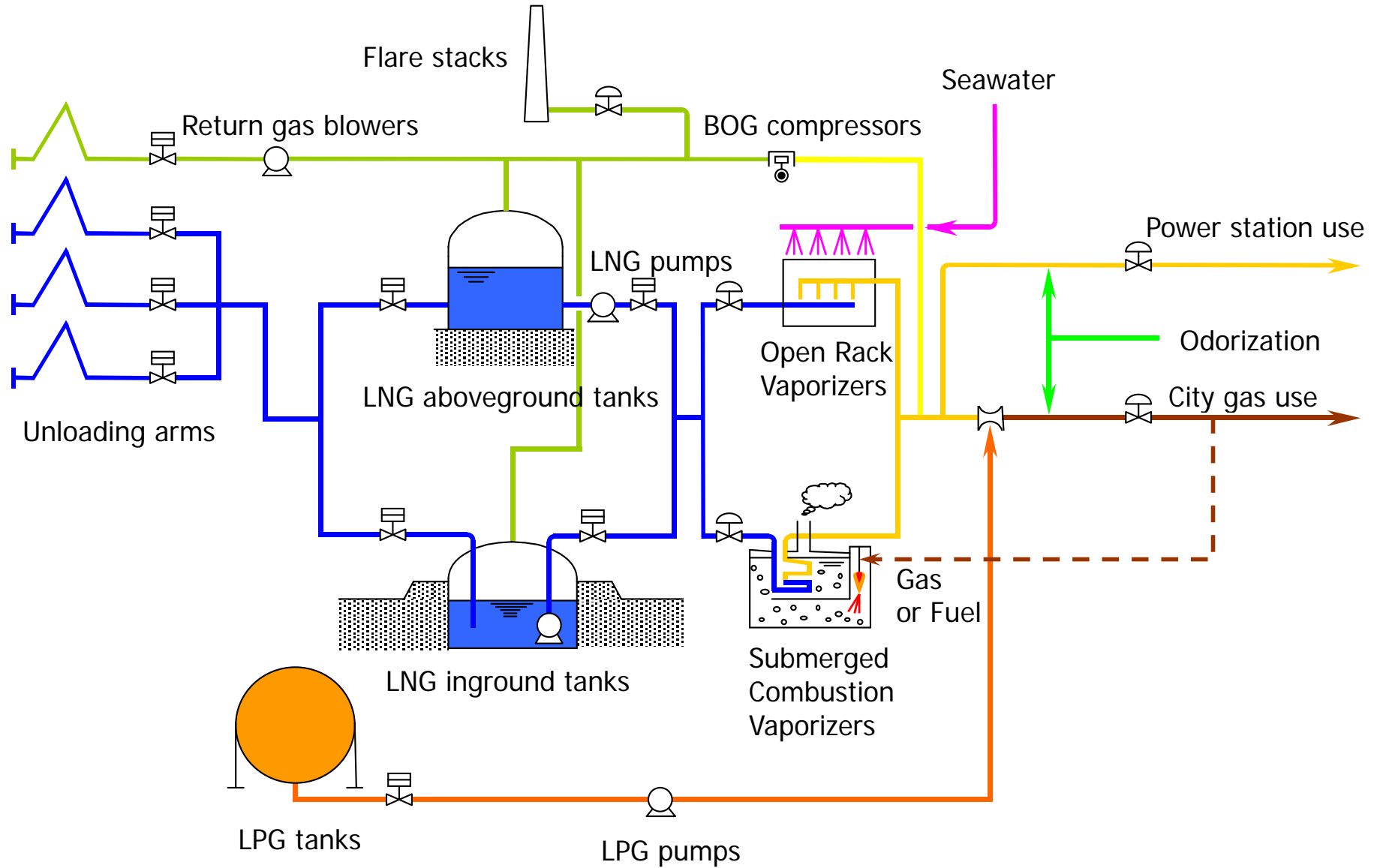
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# 2. Gas Production Process





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  - 3.1. Pressure of Trunk Line
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## 3. Quality Control of City Gas

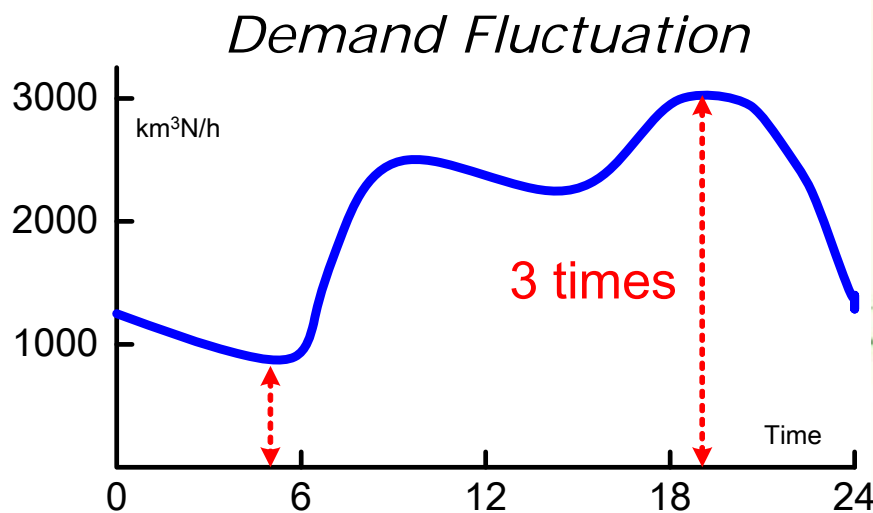
*What's the quality of city gas of Tokyo Gas?*

1. Pressure of Trunk Line
2. Calorific Value
3. Odorant

# 3.1 Pressure of Trunk Line



- **Demand fluctuation**  
(3 times difference in a day)
- **Small absorber**  
(30 small gas holders)  
(no underground storage)

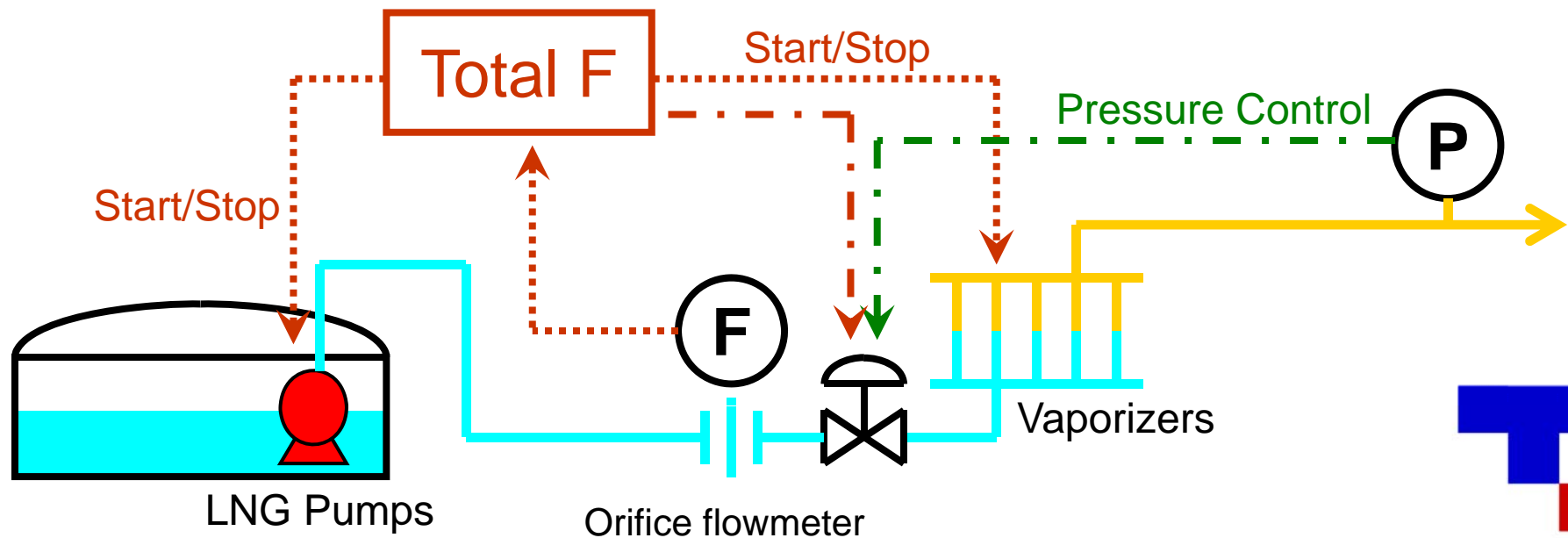


# 3.1 Pressure <Control>

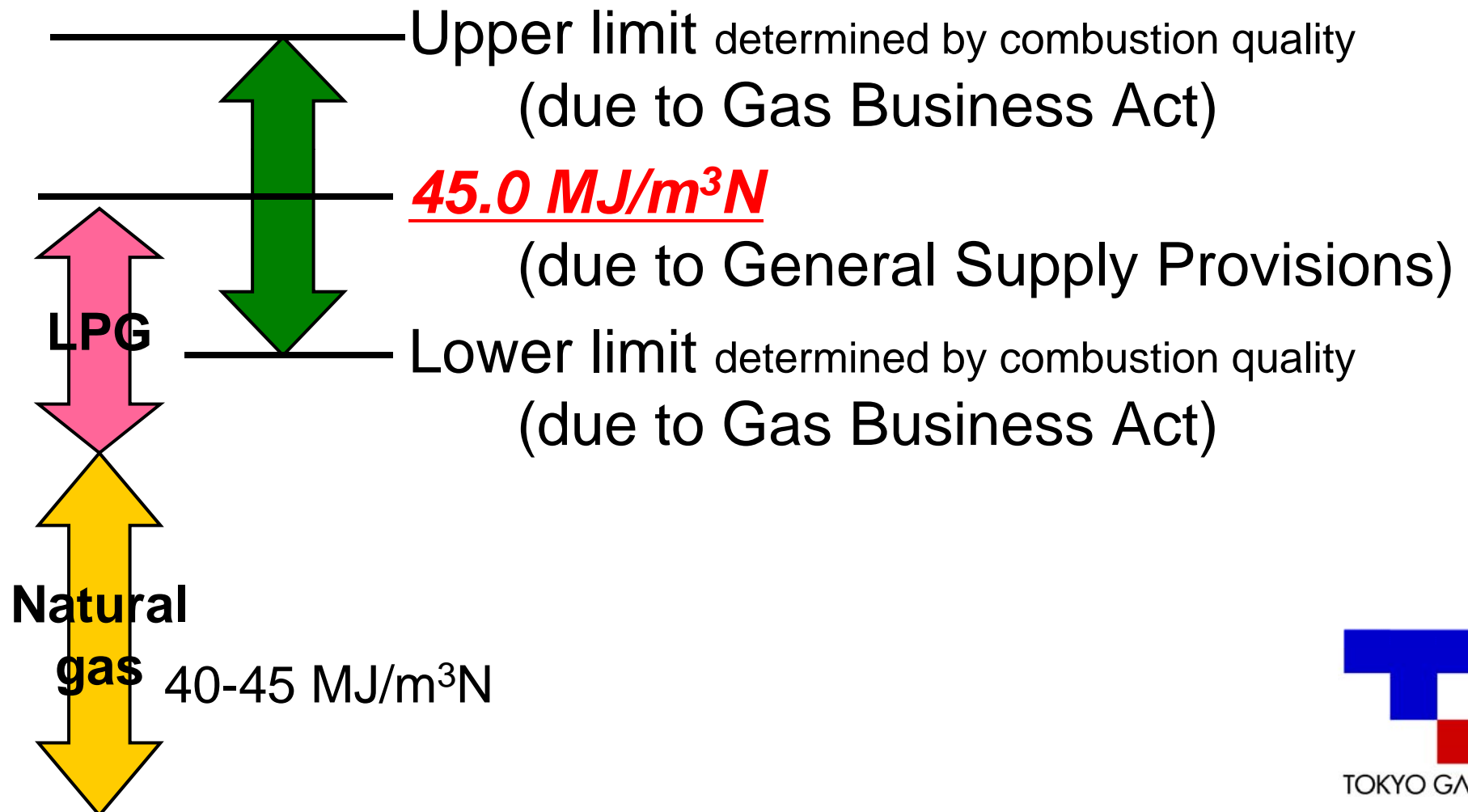
Start/Stop

## ■ Automatic Control

- Pressure Control
- Number of Pumps
- Number of Vaporizers



## 3.2 Calorific Value <Standard>

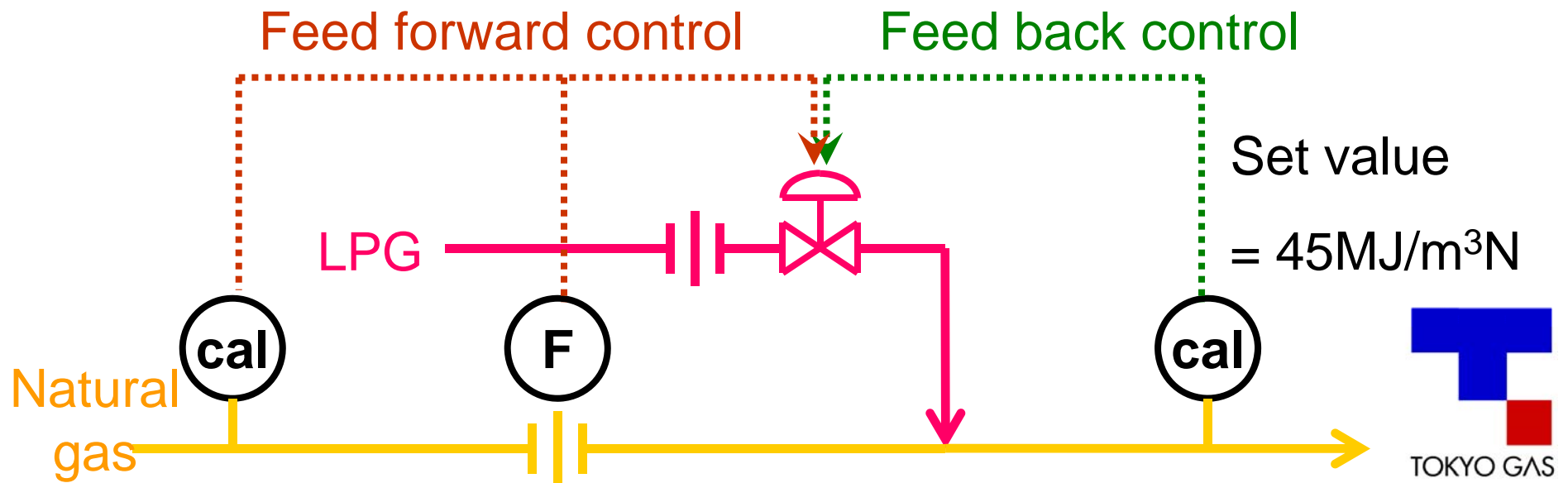




## 3.2 Calorific Value <Control>

### ■ Calorific Value Control

- Feed Forward Control
- Feed Back Control



## 3.2 Calorific Value <Instrument>

- **Calorimeter for calorific value control**  
is required “Quick Response”.  
= Vibration type gas density analyzer
- **Calorimeter for guarantee of quality**  
is required “High Accuracy”.  
= Gas Chromatography



## 3.2 Calorific Value <Issue>

### ■ Vibration type gas density analyzer

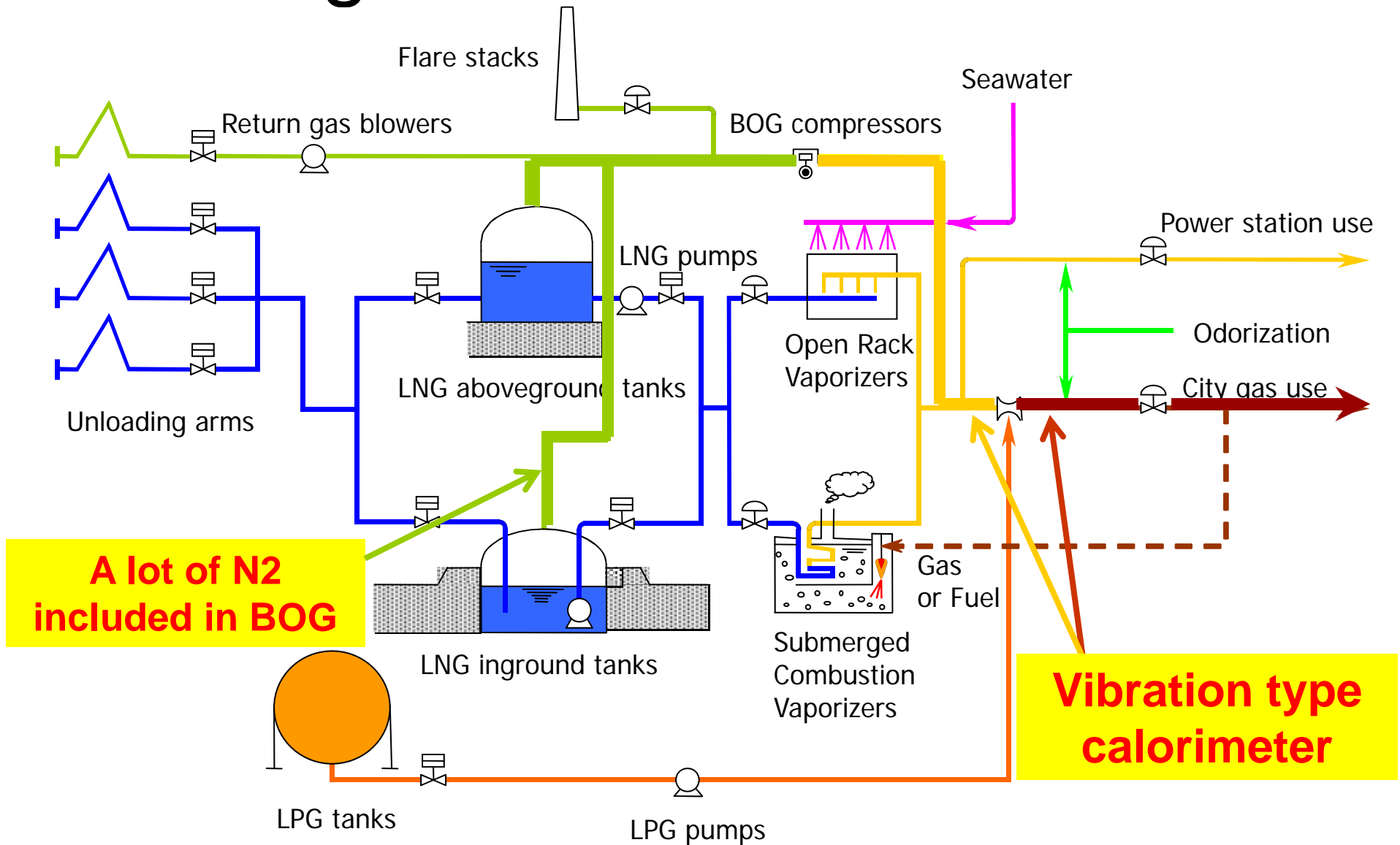
#### <Principle>

Proportional relationship  
between density and calorie of Hydrocarbon

#### <Issue>

Error caused by inert gas  
(1 % of N<sub>2</sub> = 0.65 MJ/m<sup>3</sup>N error)

# <Nitrogen in Boil Off Gas>



## 3.2 Calorific Value <Approach>

The error caused by  $N_2$  can be removed by  
<Combination of two types of calorimeter>

- **Vibration type gas density analyzer**
- **Optical Interferometric calorimeter**

<Principle>

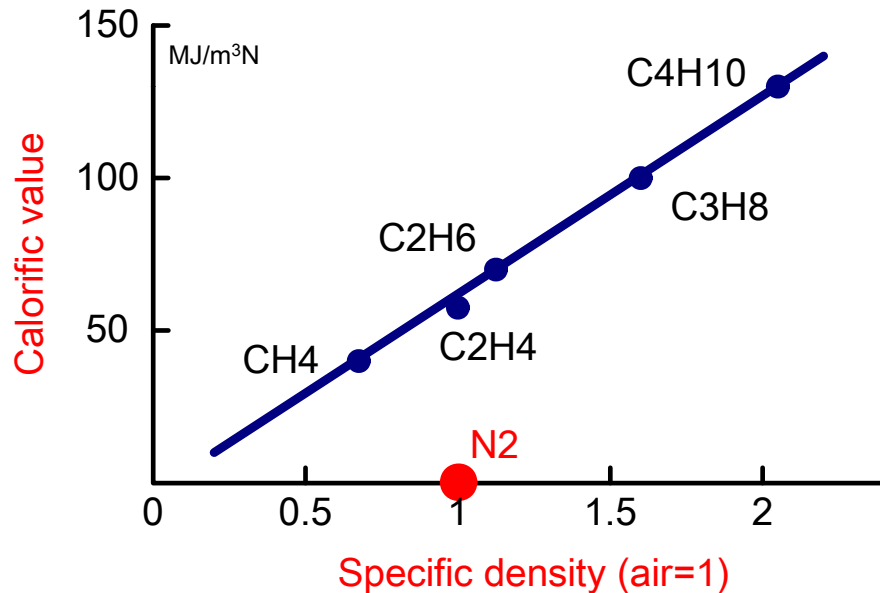
Proportional relationship

between refractive index and calorie of hydrocarbon

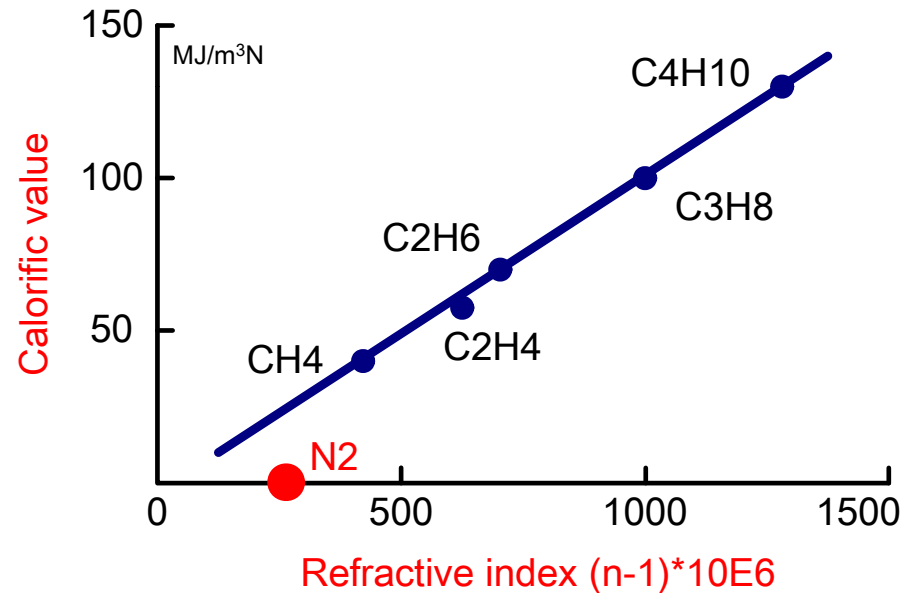
# 3.2 Calorific Value <Approach>

## ■ <Principle to remove the error>

Vibration type density analyzer



Optical Interferometric calorimeter



Nitrogen looks like to have...

65 MJ/m<sup>3</sup>N in vibration type density analyzer

26 MJ/m<sup>3</sup>N in optical interferometric calorimeter

## 3.2 Calorific Value <Approach>

### ■ <Principle to remove the error>

$$Q = Q_{vibration} - kx_{N_2}$$

$$Q = Q_{refractive} - k'x_{N_2}$$

$k$  : 0.65 MJ/m<sup>3</sup>N by 1% N<sub>2</sub>

$k'$  : 0.26 MJ/m<sup>3</sup>N by 1% N<sub>2</sub>

$x$  : contents of N<sub>2</sub> [%]

$$Q = Q_{refractive} - \frac{Q_{refractive} - Q_{vibration}}{1 - \frac{k}{k'}}$$

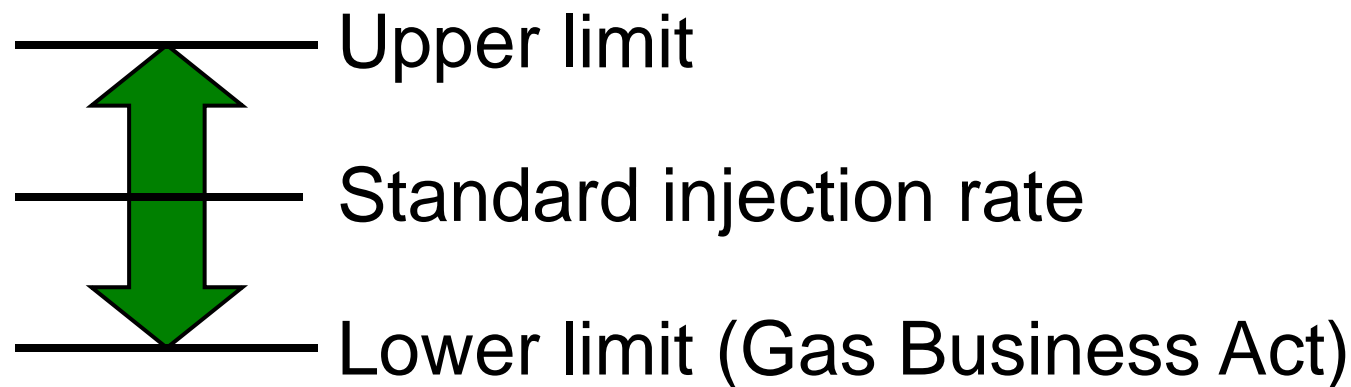
Manufactured by RIKEN KEIKI Co., LTD

## 3.3 Odorant <Standard>

### ■ Odorant

TBM (Tertiary-Butyl Mercaptan )

CH (CycloHexene)





## 3.3 Odorant <Control>

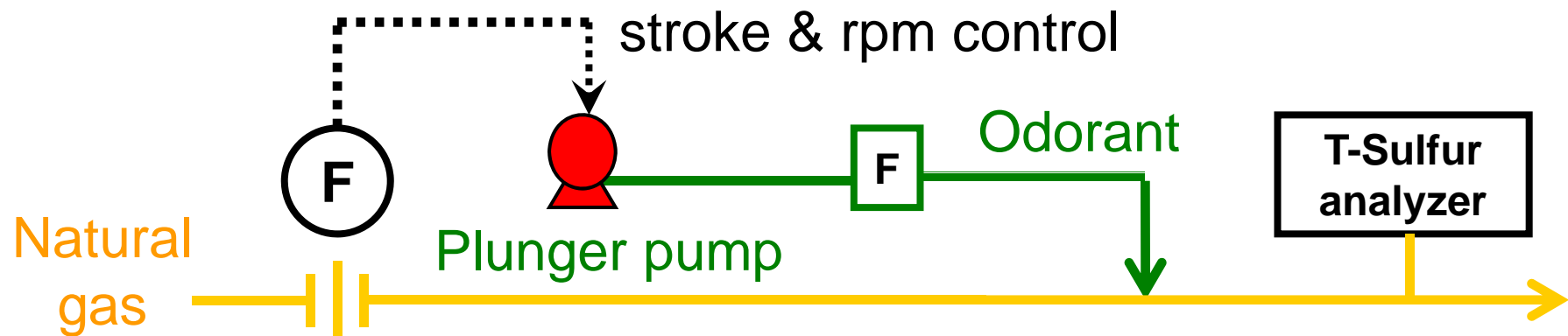
### ■ Odorant Control

Pump Output Control According to the Natural Gas Flow Rate  
(No Feed Back Control)

### ■ Measurement Points

Mass Flow Rate of Odorant

Total Sulfur in Odorized City Gas



## 3.3 Odorant <Instruments>

### <Measurement Points>

- Flowmeter of Odorant  
is required to measure “Minute Mass Flow”.  
= Coriolis flowmeter
- Total Sulfur in Odorized City Gas  
is required to measure total sulfur  
= Ultraviolet Fluorescence Method sulfur analyzer



*Thank you for your kind attention !*

*Please contact me if you have any questions.*

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